

计算凝析油当量气体体积的方法及应用

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内容提要 本文提供了计算凝析油当量气体体积的方法,并用于凝析气藏的凝析油含量、凝析油和干气地质储量的计算。

主题词 凝析气藏 凝析油 干气 含量 当量 储量

凝析气藏是一种特殊的气藏。在原始地层条件下,对于原始地层压力大于露点压力的未饱和凝析气藏,其烃类以单相气体存在于地层之中。当凝析气藏的流体通过气井采至地面时,经一级或二级分离器的作用,由于压力和温度的下降,而发生凝析油的析出,并分别计量出天然气(干气)和凝析油的产量。

对于原始地层压力等于露点压力的饱和凝析气藏,地层中的烃类仍以单相气体存在。而当地层压力低于露点压力之后,在地层中将会发生反凝析现象。此时,在地面采出的凝析油含量和凝析油的相对密度,随地层压力

的下降会逐步变小;而凝析气油比会随之变大。

对于原始地层压力低于露点压力的凝析气藏,在原始条件下,就有轻质油环或油底的存在。这种饱和型的凝析气藏,可以是大气顶小油环小油底,或小气顶大油环大油底。同时,油环、油底的轻质油具有很强的挥发性,因而俗有易挥发油之称。

对于新发现的凝析气藏,在初期进行油气藏评价时,都会遇到计算凝析油含量、凝析油和天然气(干气)的地质储量问题,而这种计算都要涉及到凝析油当量气体体积的大

二者总的效果接近;锥形的脉冲射流特性较差。

(4)泵压大于10MPa时,上喷嘴的流道形状最好选用锥形;泵压小于10MPa时,上喷嘴流道形状最好选用流线性。

(5)在实验范围内,泵压与脉冲射流特性成正比,即泵压越高,脉冲射流特性越好。最低起始脉冲泵压为1.89MPa。

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小。本文将对计算凝析油当量气体体积的方法进行必要的推导,并介绍如何用于凝析油含量、凝析油和干气地质储量的计算方法。

凝析油当量气体体积的计算方法

根据液体密度的定义,地面凝析油和净水的密度可分别写为:

$$\rho_o = m_o/V \quad (1)$$

$$\rho_w = m_w/V \quad (2)$$

式中 ρ_o ——凝析油的密度, kg/m^3 ;

ρ_w ——净水的密度, kg/m^3 ;

m_o ——凝析油的质量, kg ;

m_w ——净水的质量, kg ;

V ——体积, m^3 。

又根据液体相对密度的定义,凝析油的相对密度(γ_o)可表示为:

$$\gamma_o = \rho_o/\rho_w = m_o/m_w \quad (3)$$

已知 1m^3 净水的质量等于 1000kg , 故由(3)式可得 1m^3 凝析油的质量为:

$$m_o = 1000\gamma_o \quad (4)$$

如果凝析油的分子量以 M_o 表示, 那么, 1m^3 凝析油的摩尔数(n_o)表示为:

$$n_o = m_o/M_o = 1000\gamma_o/M_o \quad (5)$$

应当指出, 当物质的量用摩尔(mol)表示之后, 已与物质的状态(是气态或液态)无关。

根据气体分子物理学可知, 在 0.101MPa 和 273K 的条件下, 1kmol (千摩尔) 气体所占有的体积为 22.414m^3 。如果改为地面标准条件, 即 0.101MPa 和 293K , 那么, 1kmol 气体所占有的体积为:

$$V_{sc} = \frac{22.414 \times 293}{273} = 24.056\text{m}^3$$

因此, 拥有 n_o 千摩尔的 1m^3 凝析油的当量气体体积(GE_o), 存在如下的正比关系:

$$1\text{kmol} : n_o = 24.056 : GE_o \quad (6)$$

$$\text{或写为 } GE_o = 24.05n_o \quad (7)$$

将(5)式代入(7)式得:

$$GE_o = \frac{24056\gamma_o}{M_o} \quad (8)$$

当缺少凝析油分子量的取样分析数据时, 还可采用如下的相关经验公式计算⁽¹⁾:

$$M_o = \frac{44.29\gamma_o}{1.03 - \gamma_o} \quad (9)$$

通过凝析油的当量气体体积, 可以将地面采出的凝析油体积量, 换算为地面标准条件下的干气气体体积量。

凝析油含量的计算方法

对于凝析气藏的气井, 采至地面的流体(简称为井流), 经分离器分离之后, 可以分别得到在地面标准条件下, 干气和凝析油的产量。若利用凝析油当量气体体积, 将凝析油的体积换算为干气的体积时, 那么, 气井的总产气量可表示为:

$$q_{gt} = q_g + q_o GE_o \quad (10)$$

式中 q_{gt} ——气井的总产井流量, m^3/d ;

q_g ——气井的干气(天然气)产量, m^3/d ;

q_o ——气井的液体凝析油产量, m^3/d ;

GE_o ——凝析油的当量气体体积, m^3/m^3 。

将(10)式改写为下式:

$$q_{gt}/q_o = GOR + GE_o \quad (11)$$

式中的 GOR 为原始油气比(q_g/q_o), 单位表示为 m^3/m^3 。

根据凝析油含量的定义, 将(11)式取倒数后, 即得计算凝析油含量的关系式为:

$$\delta = \frac{q_o}{q_{gt}} = \frac{1}{GOR + GE_o} \quad (12)$$

式中 δ 为凝析油含量, 单位以 m^3/m^3 表示。

在矿场实际应用时, 由于凝析油的含量较小, 用 m^3 单位表示不方便, 而常用 cm^3 的单位表示。已知 $1\text{m}^3 = 10^6\text{cm}^3$, 因此(12)式可

写为:

$$\delta = \frac{10^6}{GOR + GE_0} \quad (13)$$

若凝析油的含量用 g/m^3 单位表示,则(13)式再乘以凝析油的地面密度得:

$$\delta = \frac{10^6 \rho_0}{GOR + GE_0} \quad (14)$$

式中凝析油密度(ρ_0)的单位为 g/cm^3 。

凝析油和干气地质储量的计算方法

凝析气藏的总地质储量可表示为:

$$G_{gt} = G_g + 10^{-4} N_0 GE_0 \quad (15)$$

式中 G_{gt} —— 凝析气藏的总地质储量, 10^8m^3 ;

G_g —— 凝析气藏的干气地质储量, 10^8m^3 ;

N_0 —— 凝析气藏的凝析油地质储量, 10^4m^3 。

由(15)式得凝析油的地质储量为:

$$N_0 = \frac{10^4 G_{gt}}{GOR + GE_0} \quad (16)$$

$$GOR = 10^4 G_g / N_0 \quad (17)$$

式中的 GOR 为原始气油比,单位以 m^3/m^3 表示。

凝析气藏的总地质储量,以容积法表示为:

$$G_{gt} = 0.01 Ah \varphi S_{g1} \frac{T_{sc} p_i}{T p_{sc} Z_1} \quad (18)$$

式中 A —— 含气面积, km^2 ;

h —— 有效厚度, m ;

φ —— 有效孔隙度, f ;

S_{g1} —— 原始含气饱和度, f ;

T —— 地层温度, K ;

T_{sc} —— 地面标准温度, K ;

p_{sc} —— 地面标准压力, MPa ;

p_i —— 原始地层压力, MPa ;

Z_1 —— 原始气体偏差系数。

当由(16)式求得凝析油的地质储量之

后,由(17)式得计算干气地质储量为:

$$G_g = 10^{-4} N_0 GOR \quad (19)$$

式中各参数的单位同前所注。

在凝析气藏的总地质储量中,干气地质储量所占的分量,由(15)式得:

$$f_g = 1 - \frac{10^{-4} N_0 GE_0}{G_{gt}} \quad (20)$$

方法应用举例

已知某凝析气藏的基础资料如下^[1]:

原始地层压力, $p_i = 20.684 \text{MPa}$; 地层温度, $T = 115.6^\circ\text{C} = 388.6 \text{K}$; 平均孔隙度, $\varphi = 0.30$; 平均束缚水饱和度, $S_{w1} = 0.27$; 平均原始含气饱和度, $S_{g1} = 0.73$; 凝析油产量, $q_o = 51.35 \text{m}^3/\text{d}$; 经分离器和油罐二级分离的干气产量, $q_g = 111400 \text{m}^3/\text{d}$; 原始生产气油比, $GOR = 2169.4 \text{m}^3/\text{m}^3$; 地面凝析油的密度, $\rho_0 = 0.8017 \text{g}/\text{cm}^3$; 地面凝析油的相对密度(水=1.0), $\gamma_0 = 0.8017$; 分离器和油罐二级分离产气量的平均干气相对密度(空气=1.0), $\gamma_g = 0.677$; 井流的相对密度(空气=1.0), $\gamma_w = 0.9267$; 井流凝析气的原始气体偏差系数, $Z_1 = 0.84$; 地面标准压力, $p_{sc} = 0.101 \text{MPa}$; 地面标准温度, $T_{sc} = 293 \text{K}$; 假定凝析气藏的面积和厚度分别为: $A = 20 \text{km}^2$; $h = 10 \text{m}$; 试求该凝析气藏的 GE_0 、 δ 、 G_{gt} 、 N_0 、 G_g 和 f_g 的数值各为多少?

将已知参数代入(9)式得凝析油的分子量为:

$$M_0 = \frac{44.29 \times 0.8017}{1.03 - 0.8017} = 155.5 \text{kg}/\text{kmol}$$

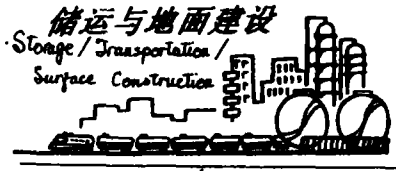
将 M_0 和 γ_0 的数值代入(8)式得凝析油的气体当量体积为:

$$GE_0 = 24056 \times 0.8017 / 155.5 = 124.02 \text{m}^3/\text{m}^3$$

将 GOR 、 GE_0 和 ρ_0 的数值代入(14)式,得到凝析油的含量为:

$$\delta = \frac{10^6 \times 0.8017}{2169.4 + 124.02} = 349.6 \text{g}/\text{m}^3$$

将已知参数代入(18)式,得凝析气藏的



液化石油气储罐 的太阳能冷却系统

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内容提要 本文针对目前国内液化石油气储罐采用淋水降温系统的特点,以及高温少雨地区太阳日照长的特点,提出用太阳能冷却系统来代替液化石油气储罐的淋水降温系统。并介绍了该方法的组成、原理和工作过程,以及主要设备和设计计算参数的计算方法。

主题词 液化石油气 储罐 太阳能 冷却系统 设计方法

目前国内均使用压力容器储存液化石油气,即采用常温高压储存法^[1]。这种储存方法有许多优点,如简单易行,投资费用省等。但是这种储存方法的最大缺点是罐内液化石油气受日照影响很大,容易造成液化石油气储罐的呼气损耗。为了解决这个问题,国内的常见方法是在液化石油气储罐上设一套淋水降

温系统或加绝热层,如南充炼油厂的液化石油气储罐(卧式罐)就设有淋水降温系统。每年夏季都要启用。采用上述这两种方法是可以达到保持罐内液化石油气的温度基本稳定这一目的,但是它们均有一些不可弥补的缺点。此外绝热材料费用和施工费用较高。淋水降温需耗用大量的清水,这对北方干旱少

总地质储量为:

$$G_{\text{总}} = 0.01 \times 20 \times 10 \times 0.30 \times 0.73$$

$$\left(\frac{293}{388.6 \times 0.101} \right) \left(\frac{20.684}{0.840} \right) = 80.5 \times 10^6 \text{m}^3$$

将 $G_{\text{总}}$ 、 GOR 和 GE_0 的数值代入(16)式得凝析油的地质储量为:

$$N_0 = \frac{10^4 \times 80.5}{2169.4 + 124.02} = 351 \times 10^4 \text{m}^3$$

将 N_0 和 GOR 的数值代入(19)式得凝析气藏干气的地质储量为:

$$G_{\text{干}} = 10^{-4} \times 351 \times 2169.4$$

$$= 76.15 \times 10^6 \text{m}^3$$

最后,将 $G_{\text{干}}$ 、 N_0 、 GE_0 和 $G_{\text{总}}$ 的数值代入(20)式,得在凝析气藏中干气地质储量占的分量为:

$$f_{\text{干}} = 1 - \frac{10^{-4} \times 351 \times 124.02}{80.5}$$

$$= 0.9495 \text{ 或 } 94.95\%$$

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Kuang Jianchao, Shi Naiguang and Yang Zhengwen: A Optimization Way of Synthesizing Overall Target Function to Calculate Reserve and Water Influx of Water Drive Gas Reservoir, NGI 13(6), 1993: 41~47

The method of calculating the reserve and water influx of water drive gas reservoir by using material balance method is improved. The optimum way of synthesizing overall target function is proposed which is, after calculating a vast amount of good schemes, through placing them in a competition by using relative Hamming distance and correlatively analysis to choose out the best one.

Subject Headings: water drive gas reservoir, synthesizing overall target, function, reserve, water influx, optimum way, optimum scheme choice.

DRILLING/PRODUCTION TECHNOLOGY AND EQUIPMENT

Zhong Bin and Liu Xuquan: U Shape Tube Effect in the Process of Cementing, NGI 13(6), 1993: 47~50

The reason of producing U shape tube effect in cementing process is analyzed in this paper. A mathematical model of the whole cementing process is set up to calculate the concrete instance and study the relevant factors thoroughly.

Subject Headings: cementing, U shape tube effect, mathematical model.

Jiang Wei: Application of Top Drive Drilling in Area 36—1, NGI 13(6), 1993: 51~53

The top drive drilling technique was applied in the oil field SZ36—1 in Liaodong Bay of Bohai and its advantages are able to shorten drilling cycle and save drilling cost as to obtain a favorable economic benefit and accelerate the proceeding of developing oil field. It is necessary to master the technique and correctively cognize its characters for developing and constructing oil field.

Subject Headings: Bohai, Liaodong Bay, oil field SZ36—1, drilling technique, drilling cost, oil field development.

Mu Fei and Song Shufang: Influence of Upper Nozzle's Passage Shapes of Pulse Nozzle on Jet Flow Properties, NGI 13(6), 1993: 53~57

This paper studies the influence of upper nozzle's passage shapes (such as streamlined, tapered, equal change speed and three times curve shapes) of pulse nozzle on jet flow properties. The result from testing can help optimizing pulse nozzle and instructing field application. The influence of pump pressure on the characters of pulse jet flow is also studied in normal pump pressure, and the priming pulse pressure of causing pulse jet flow is obtained.

Subject Headings: pulse nozzle, upper nozzle, flow passage shape, pulse range, pulse jet flow character.

Chen Yuanquan: A Method of Calculating Condensate Equivalent Gas Volume and Its Application, NGI 13(6), 1993: 57~60

A method of calculating condensate equivalent gas volume is shown in this paper. It can be used to

calculate condensate content and the geological reserves of condensate and dry gas in gas condensate reservoir.

Subject Headings: gas condensate reservoir, condensate, dry gas, content, equivalent, reserve.

STORAGE/TRANSPORTATION/SURFACE CONSTRUCTION

Ni Juanle; Solar Energy Cooldown System of Liquefied Petroleum Gas Storage Tank, NGI 13(6), 1993:60~63

Aimed at the defects of liquefied petroleum gas storage tank with drenching cooldown system at home at present, and the features of long sunshine time in high temperature & rainless area, it is put forward to replace drenching cooldown system by solar energy cooldown system. Its composition, principle, working process, main equipments and the method of designing-calculating parameters are also introduced in this paper.

Subject Headings: liquefied petroleum gas, storage tank, solar energy, cooldown system, design method.

Wang Yuchun; A New Method of Optimally Designing Transmission Line, NGI 13(6), 1993:64~69

Combining Signomial geometry program method with grey correlation analysis method, a new calculation method of optimally designing transmission line is set up and the computation software GPGR is worked out in this article. The calculation shows that the method can optimally seek out the best scheme which not only satisfies the technological requirements but is economical and reasonable. It is superior to the traditional comparison method and has application value.

Subject Headings: transmission line, optimal design, Signomial geometry program, grey correlation analysis method, computation software.

GAS PROCESSING AND CHEMICAL TECHNOLOGY

Zhang Junfeng and Zhang Hua; Super Claus Sulfur Recovery Technique, NGI 13(6), 1993:70~74

Based on introducing the principle and feature of super Claus sulfur recovery technique, this paper expounds the construction and moving situation of super Claus device abroad. It is shown changing the instruments, equipments, pipeline and control system of conventional Claus device into those of super Claus device to provide a reference for importing and transforming the existing Claus devices at home.

Subject Headings: sulfur recovering, super Claus, catalyst, device transforming.

Zhou An and Luo Guangxi; Comparing the Forecast Ways of Maximum Water Content in Natural Gas, NGI 13(6), 1993:75~78

The data from testing the hydrate balancing with natural gas water content are used to verify the